

: B8THx30/1P

SSP : B8T

		1	2
		R32	Propylene Glycol - Water (30.0 mass%)
		<b>2.000</b>	
		kW	
		°C	
		<b>43.00</b>	
		0.256	
		<b>1.000</b>	
		°C	
(poca)		3.5	<b>12.0</b>
		°C	
		<b>3.5</b>	
		K	
		<b>5.0</b>	
		°C	
		8.5	<b>7.0</b>
		kg/s	0.1047
		8.513e-3	
		kg/s	
		2.181e-3	
		kg/s	
		6.332e-3	
( C H)		kPa	
		1.04 ( <b>50.00</b> )	<b>1.47 (50.00)</b>
		1	2
		m <sup>2</sup>	0.644
		kW/m <sup>2</sup>	3.11
		K	6.7
Overall heat transfer coefficient		W/m <sup>2</sup> ,°C	464
		kPa	1.04
- ( B / * )		kPa	1.47
- ( )		-3.73e-3/0.0349	0.0869
( )		0.000 - 0.000	
( )		907	
		14	15
		30	
		7	
		0.143	
( / )		m <sup>2</sup> ,°C/kW	
		17.5/17.5	17.5/17.5
		mm	
		2.26 - 3.57	
		mm	
		4.32 - 9.67	
		41.18	
-		m/s	0.421
		1.53	
		m/s	0.0462
		0.180	
		kPa	4.41e-3
-			
/		K	0.2
-		°C	
*		4.7/11.4	4.8/11.4

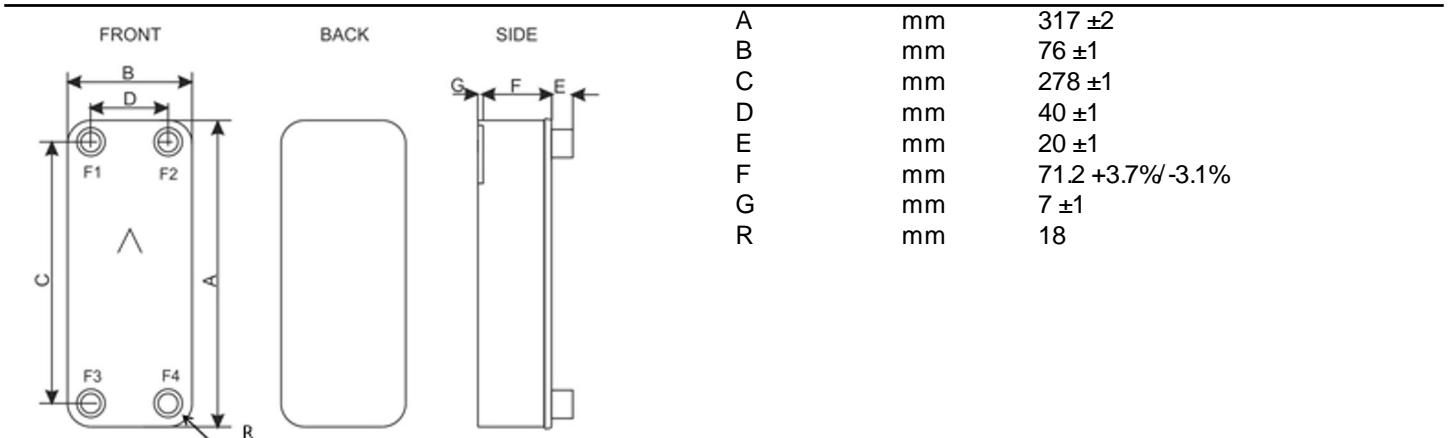
! Vapor velocity is lower than recommended, this can have impact on oil transport.

		1	2
		°C	3.5
		cP	9.4
		0.144	4.64
		kg/m <sup>3</sup>	1034
		1042	1034
		kJ/kg,°C	3.822
		1.804	3.822
		W/m,°C	0.4337
		0.1426	0.4337
		cP	
		0.0117	



	1	2
•	kg/m <sup>3</sup>	23.20
•	kJ/kg,°C	1.013
•	W/m,°C	0.01114
•	kJ/kg	309.1
• Bub Enthalpy	kJ/kg	205.7
• Dew Enthalpy	kJ/kg	517.3
• Inlet Enthalpy	kJ/kg	285.5
• Outlet Enthalpy	kJ/kg	526.3
	W/m <sup>2</sup> ,°C	4490
		2080

	1	2
( )*	kg	3.1
( )	dm <sup>3</sup>	0.55
( )	dm <sup>3</sup>	0.58
F1/P1	mm	16
F2/P2	mm	16
F3/P3	mm	16
F4/P4	mm	16



A	mm	317 ±2
B	mm	76 ±1
C	mm	278 ±1
D	mm	40 ±1
E	mm	20 ±1
F	mm	71.2 +3.7%/-3.1%
G	mm	7 ±1
R	mm	18

SWEP.

	Unit	Value
Sweden - Landskrona	kg CO <sub>2</sub> e	16.0 - 16.0
USA - Tulsa	kg CO <sub>2</sub> e	16.7 - 16.8
Slovakia - Košice	kg CO <sub>2</sub> e	18.1 - 18.2
Malaysia - Kuala Lumpur	kg CO <sub>2</sub> e	25.3 - 25.3
China - Suzhou	kg CO <sub>2</sub> e	43.3 - 43.4

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