

: B18Hx50/1P

SSP : B18H

		1	2
		R744 (Carbon Dioxide) (90.0 bar)	Propylene Glycol - Water (30.0 mass%)
		22.50	
		90.0	25.0
		30.0	45.0
		0.1018	0.2890
(C H)	kPa	0.624 (50.00)	2.11 (50.00)
		3.30	1.10
		1	2
		m ²	1.97
		kW/m ²	11.4
		K	18.2
Overall heat transfer coefficient	W/m ² ,°C	1040	
- *	kPa	0.624	2.11
-	kPa	0.0532	0.190
(/)	mm	24.0/24.0	24.0/24.0
		24	25
			50
			7
		m ² ,°C/kW	0.063
		2803	109.4
(/)	m/s	0.497/0.497	0.625/0.625
		m/s	0.0667
		kPa	4.39e-3
		°C	36.7
		K	0.9
/	°C	27.6/52.3	27.4/51.4

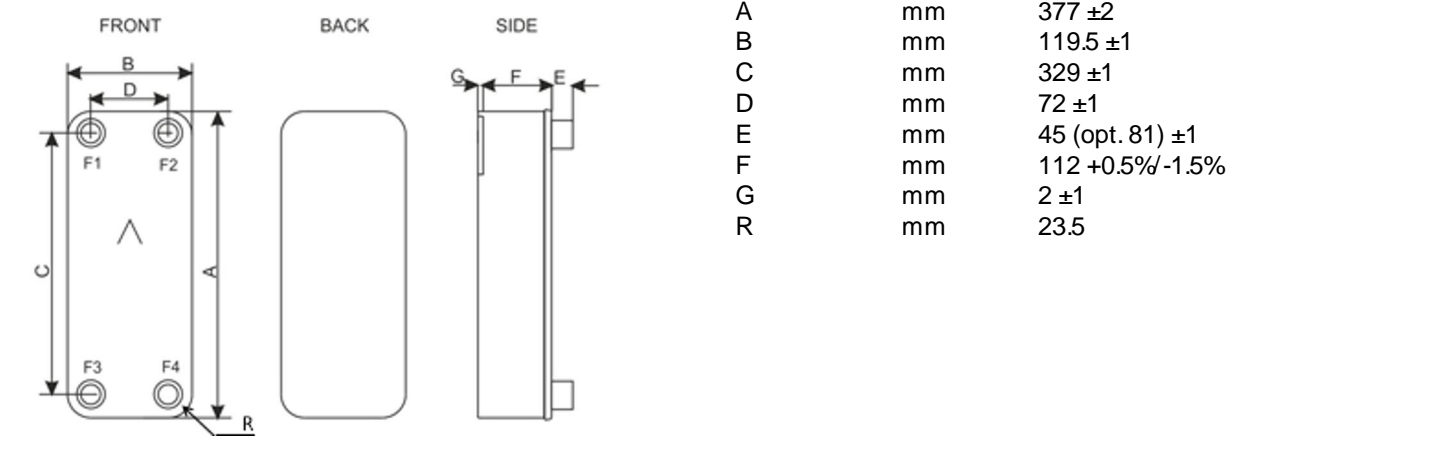
! For a desuperheater installation it is recommended to have the gas enter in the top of the BPHE, either in F1 or F2. The reason is to easily remove possible condensate from the BPHE

		1	2
		°C	43.7
		cP	0.0216
		kg/m ³	235.6
		kJ/kg,°C	2.380
		W/m,°C	0.03367
		W/m ² ,°C	1770
		1	2
()*		kg	16.57
()*		kg	18.79
()	dm ³	1.46	
()	dm ³	1.52	
F1/P1	mm	24	
F2/P2	mm	24	



		1	2
	F3/P3	mm	24
	F4/P4	mm	24

*



A	mm	377 ±2
B	mm	119.5 ±1
C	mm	329 ±1
D	mm	72 ±1
E	mm	45 (opt. 81) ±1
F	mm	112 +0.5%/-1.5%
G	mm	2 ±1
R	mm	23.5

*

SWEP.

	Unit	Value
Sweden - Landskrona	kg CO ₂ e	85.3
USA - Tulsa	kg CO ₂ e	89.5
Slovakia - Košice	kg CO ₂ e	97.0
Malaysia - Kuala Lumpur	kg CO ₂ e	135.1
China - Suzhou	kg CO ₂ e	231.7

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