

: B185Hx140/1P

SSP : B185H

| | | 1 | 2 |
|-----------------------------------|----------------------|-------------------------------------|---|
| | | R744 (Carbon Dioxide) (90.0 bar) | Propylene Glycol - Water (30.0 mass%) |
| | | 182.0 | |
| | | 95.0 | 25.0 |
| | | 30.0 | 45.0 |
| | | 0.7964 | 2.338 |
| (C H) | kPa | 3.37 (50.00) | 9.19 (50.00) |
| | | 3.33 | 1.02 |
| | | 1 | 2 |
| | | 10.4 | |
| | | 17.4 | |
| | | 19.5 | |
| Overall heat transfer coefficient | W/m ² ,°C | 1490 | |
| - * | kPa | 3.37 | 9.19 |
| - | kPa | 0.936 | 0.659 |
| (/) | mm | 33.0/33.0 | 50.0/50.0 |
| | | 69 | 70 |
| | | 140 | |
| | | 4 | |
| | | 0.024 | |
| | | 4441 | 180.3 |
| (/) | m/s | 2.07/2.07 | 1.16/1.16 |
| | | 0.171 | 0.110 |
| | | 5.37e-3 | 0.0188 |
| | | 37.2 | 36.6 |
| | | 1.3 | |
| | | 27.6/53.2 | 27.4/51.8 |

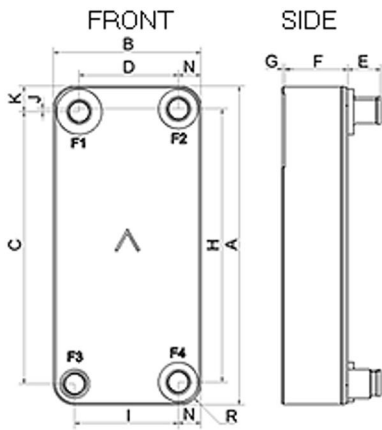
! For a desuperheater installation it is recommended to have the gas enter in the top of the BPHE, either in F1 or F2. The reason is to easily remove possible condensate from the BPHE

| | | 1 | 2 |
|-------|-----------------|---------|--------|
| | | 44.2 | 34.5 |
| | | 0.0214 | 1.84 |
| | | 227.5 | 1023 |
| | | 2.224 | 3.892 |
| | | 0.03285 | 0.4583 |
| | | 2480 | 5230 |
| | | 1 | 2 |
| ()* | kg | 72.45 | |
| ()* | kg | 84.28 | |
| () | dm ³ | 7.63 | |
| () | dm ³ | 8.18 | |
| F1/P1 | mm | 33 | |
| F2/P2 | mm | 50 | |



| | | 1 | 2 |
|--|-------|----|----|
| | F3/P3 | mm | 33 |
| | F4/P4 | mm | 50 |

*



| | | |
|---|----|----------|
| A | mm | 425.2 ±2 |
| B | mm | 203.2 ±1 |
| C | mm | 354 ±1 |
| D | mm | 126 ±1 |
| E | mm | 45 ±1 |
| F | mm | 298 ±3% |
| G | mm | 0 ±1 |
| H | mm | 342 ±1 |
| J | mm | 6 |
| K | mm | 35.6 |
| N | mm | 41.6 |
| R | mm | 41.6 |

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SWEP.

| | Unit | Value |
|-------------------------|----------------------|---------|
| Sweden - Landskrona | kg CO ₂ e | 373.1 |
| USA - Tulsa | kg CO ₂ e | 391.3 |
| Slovakia - Košice | kg CO ₂ e | 424.3 |
| Malaysia - Kuala Lumpur | kg CO ₂ e | 590.8 |
| China - Suzhou | kg CO ₂ e | 1,013.5 |

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